

# Electronic Supplementary Material

## Mechanism of ethanol/water separation through functional graphene membrane: a molecular simulation investigation

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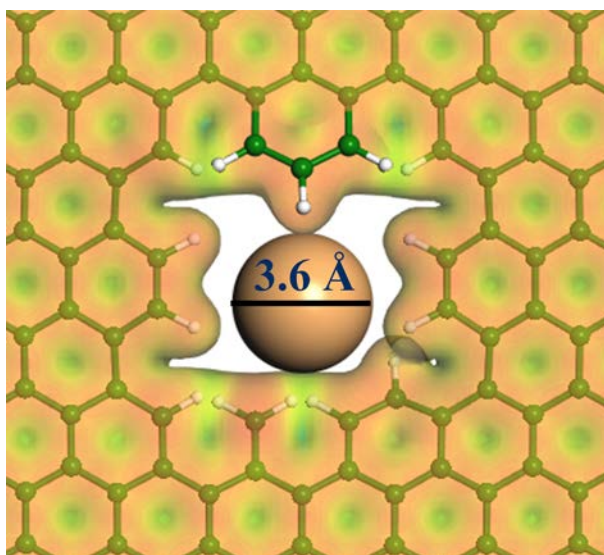
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### 1. The criterion for the diameter definition of nanopores

Fig. S1 shows the criterion for the diameter definition of nanopores. Taking the PG\_D3.6Å as an example, the pore size is defined as the diameter of an inserted sphere that is inserted in the pores without contact with membrane atoms [1, 2].



**Fig. S1.** The criterion for the diameter definition of the nanopore in PG\_D3.6Å.

### 2. Comparison of pervaporation performance

The reversed separation performance of our designed membrane is compared with both polymeric and inorganic membranes. In Table S1, all fluxes are normalized by the transmembrane pressure as per previous studies [2,3]. The designed PG\_D3.8Å shows promising performance for ethanol/water separation with ethanol permeance and its separation factor up to  $11.5 \times 10^3$  GPU (i.e.,  $69.3 \text{ kg} \cdot \text{m}^{-2} \cdot \text{h}^{-1} \cdot \text{bar}^{-1}$ ) and 34, which is comparable to previous experiments.

**Table S1** Performance comparison.  $S_{e/w}$  is the separation factor of ethanol over water, and  $F_e$  and  $P_e$  are ethanol contents in the feed and permeate sides, respectively.

Membrane	Temp. (°C)	$F_e$ (wt%)	Total flux ( $\text{kg} \cdot \text{m}^{-2} \cdot \text{h}^{-1}$ )	$S_{e/w}$	$P_e$ (wt%)	Ethanol permeance (GPU)	Ref.
PDVB/PDMS	60	6	1.423	10.0	39.0	1885.8	[4]
BTESO/silicalite-1	60	5	6.84	24.6	56.4	15442.9	[5]
W-MFI zeolite	60	5	2.81	32.0	62.7	7055.2	[6]
ZIF-91/PDMS-20	55	5	0.846	15.8	45.4	1950.5	[7]
AZIF-8@PDMS	40	5	0.5856	17.7	48.2	3093.1	[8]
PDMS/ZIF-8@GO	40	5	0.4438	22.2	53.9	2619.0	[9]
ZIF-8@PDMS	40	5	1.778	12.1	38.9	7576.1	[10]
ODPA-ZIF-8(4)@ZIF-8/PDMS	30	5	0.64	17.4	47.8	5877.4	[11]
silicalite-1	50	10	4.47	66.0	88.0	14021.6	[12]
PTMSP	40	10	0.19	8.3	48.0	545.1	[13]
PDMS/PVDF	30	10	0.085	6.0	40.0	355.1	[14]
PG_D3.8Å	27	10	87.6	34.0	79.0	11542.8	<b>This work</b>

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