
Electronic Supplementary Material

Floret-like Fe-N_x nanoparticle-embedded porous carbon superstructures from a Fe-covalent triazine polymer boosting oxygen electroreduction

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Experimental methods

Materials

Cyanuric chloride (99%), piperazine (99%) and triethylamine (99.5%), iron (III) chloride (98%) were obtained from Aladdin Reagent Co, Ltd, China. Acetonitrile (AR, $\geq 99.0\%$), triethylamine (AR, $\geq 99.0\%$), acetone (AR, $\geq 99.0\%$), ethanol (99.5%), H₂SO₄ (AR, 95.0 ~ 98.0%) and zinc acetate dihydrate (AR, $\geq 99.0\%$) were purchased from Sinopharm Chemical Reagent Co, Ltd, China. Potassium hydroxide (KOH, GR, $\geq 90\%$) and nafion solution (5 wt%) were purchased from Sigma-Aldrich Co. Ltd. 20 wt% commercial Pt/C catalyst was purchased from Alfa Aesar chemical Co, Ltd, China. All these chemicals were used as received without further purification unless specified. Deionized water was produced by a laboratory water maker at 25 °C (18.2 M Ω ·cm⁻¹ resistivity) and used throughout the experiments.

Characterizations

The solid-state ¹³C nuclear magnetic resonance spectrum was confirmed on an AvanceIII400MHz instrument (Germany) with tetramethylsilane (TMS) as an internal standard. Fourier transform infrared spectrometer (FT-IR) spectra were measured utilizing a Perkin-Elmer Instrument. The X-ray photoelectron spectroscopy (XPS) was recorded on a Karatos Axis ULTRA spectrometer. The nitrogen adsorption and desorption isotherms were conducted at the liquid nitrogen (77 K) with a QUADRASORB SI automated surface area and pore size analyzer device (Quantachrome Corporation, USA), the specific surface area (SSA) of CTPS and resultant catalysts were received from the adsorption curves based on the Brunauer-Emmett-Teller (BET) equation and the calculation of pore-size distribution of samples were received, which were based on nonlocal density functional theory (DFT) equilibrium model. Before measurements, all the samples were outgassed at 120 °C in vacuum for 24 h. Raman spectra were carried out on a LabRAM ARAMIS system with a wavelength 633 nm laser. Powder X-ray diffraction (XRD) patterns of samples were received at an X-ray diffractometer on a Bruker D8 Advance. TGA was performed on TG 209 F1 from room temperature to 1000 °C in N₂ atmosphere with a heating rate of 10 °C min⁻¹. The

surface morphologies of the metal-coordinated polymer precursors and corresponding carbon catalysts were observed by field-emissions scanning electron microscopy (JEOL JSM-7500F) at an accelerating voltage of 5.0 kV. Transmission electron microscopy (TEM) was conducted through Talos F200S.

Electrochemical measurements

The ORR electrocatalytic activities of the catalysts were performed with CHI 660D electrochemical workstation in a standard three-electrode system using a graphite rod as the counter electrode, and the 5 mm diameter rotating disk electrode (RDE, Gamry Instruments, Inc.) loaded with catalysts as the working electrode. The catalyst ink was prepared by dispersing 5 mg of the catalysts into 350 μL of ethanol and 95 μL of Nafion solution (5 wt%). After sonication for 30 min, 5 μL catalyst ink was deposited onto the RDE ($\sim 290 \mu\text{g cm}^{-2}$ mass loading) and dried at room temperature naturally. For comparison, commercial Pt/C catalysts were used as a reference under same condition.

Rotating disk electrode (RDE) test: The ORR activities of catalysts were evaluated by cyclic voltammetry (CV) and linear sweep voltammetry (LSV) at the rotation rate of 800, 1200, 1600, 2000 and 2400 rpm, respectively, with O_2 -saturated 0.1 M KOH solution as the electrolyte. All the potentials are transformed into a reference hydrogen electrode (RHE) using the following equations:

$$E \text{ (vs. RHE)} = E \left(\text{vs. } \frac{\text{Ag}}{\text{AgCl}} \right) + 0.197 + 0.059 \times \text{pH}$$

The polarization curves were carried out in 0.1 M O_2 -saturated KOH electrolyte with a potential range from -0.2 V to 1.2 V (vs. RHE) at a rotation speed of 1600 rpm. Before the RDE test, the electrodes were scanned for 100 CV cycles with a scan rate of 100 mV s^{-1} in O_2 -saturated 0.1 M KOH to activate the catalyst. The electron transfer number (n) was calculated by linear fitting using the Koutecky-Levich (K-L) equation:

$$\frac{1}{j} = \frac{1}{B\omega^{1/2}} + \frac{1}{j_K}$$
$$B = 0.62nFC_0(D_0)^{2/3}\nu^{-1/6}$$

where j is the measured current density, F is the Faraday constant ($F = 96485 \text{ C cm}^{-1}$), C_0 is the bulk concentration of O_2 ($C_0 = 1.2 \times 10^{-3} \text{ M}$), D_0 is the diffusion coefficient of oxygen (D_0

$= 1.9 \times 10^{-5} \text{ cm s}^{-1}$) in a 0.1 M KOH solution, ν is the kinetic viscosity of the electrolyte ($0.01 \text{ cm}^2 \text{ s}^{-1}$), and k is the electron transfer rate constant. The value of B can be obtained from the slope of the K-L equation, and ω is the rotation rate. Thus, when B is known, the electron transfer number (n) can be calculated from the equation.

Rotating ring-disk electrode (RRDE) test: The catalytic performance of the catalyst towards ORR was performed via cyclic voltammetry (CV) at a scan rate of 50 mV s^{-1} and linear sweep voltammetry (LSV) at a scan rate of 5 mV s^{-1} on a rotating ring-disk electrode (RRDE), and ring electrode was also scanned. The yield of hydrogen peroxide and electron transfer number (n) were obtained from the equations as follows:

$$\text{H}_2\text{O}_2 (\%) = 200 \cdot \text{I}_r / \text{N} / (\text{I}_d + \text{I}_r / \text{N})$$

$$n = 4 \cdot \text{I}_d / (\text{I}_d + \text{I}_r / \text{N})$$

in which I_d and I_r represent the disk and ring currents, and N is corresponding to the ring collection efficiency, which is provided as 0.37 by manufacture.

Zn-air battery measurements

The conventional Zn-air batteries were fabricated using a self-made acrylic resin cell and the measurements were conducted under ambient conditions. A hydrophobic carbon paper was provided as the current collector. A polished zinc plate (0.20 mm thickness) and 6.0 M KOH solution containing 0.2 M zinc acetate are served as the anode and electrolyte, respectively. The cathode was prepared with loading Fe/N@CNF-800 or commercial Pt/C catalysts on the $1 \times 1 \text{ cm}$ carbon cloth ($\sim 1.0 \text{ mg cm}^{-2}$).

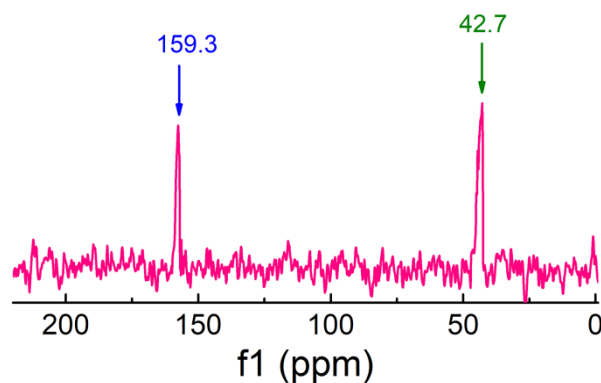


Fig. S1. Solid-state ^{13}C NMR spectrum of CTP.

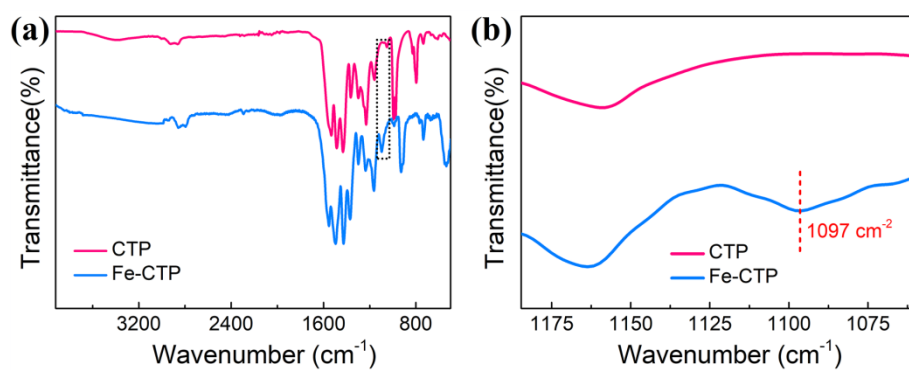


Fig. S2. FT-IR spectrum of Fe-CTP and CTP.

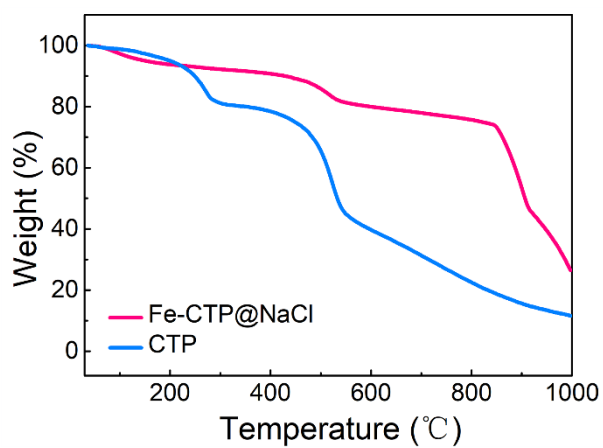


Fig. S3. TGA curves of the Fe-CTP@NaCl and CTP.

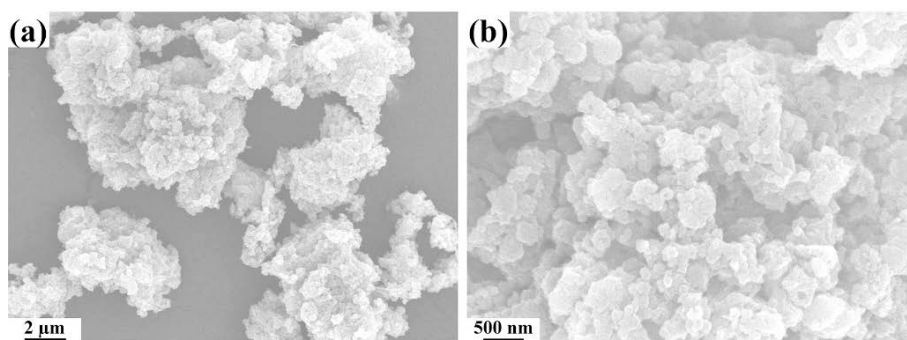


Fig. S4. SEM images of Fe-CTP at low and high magnifications, respectively.

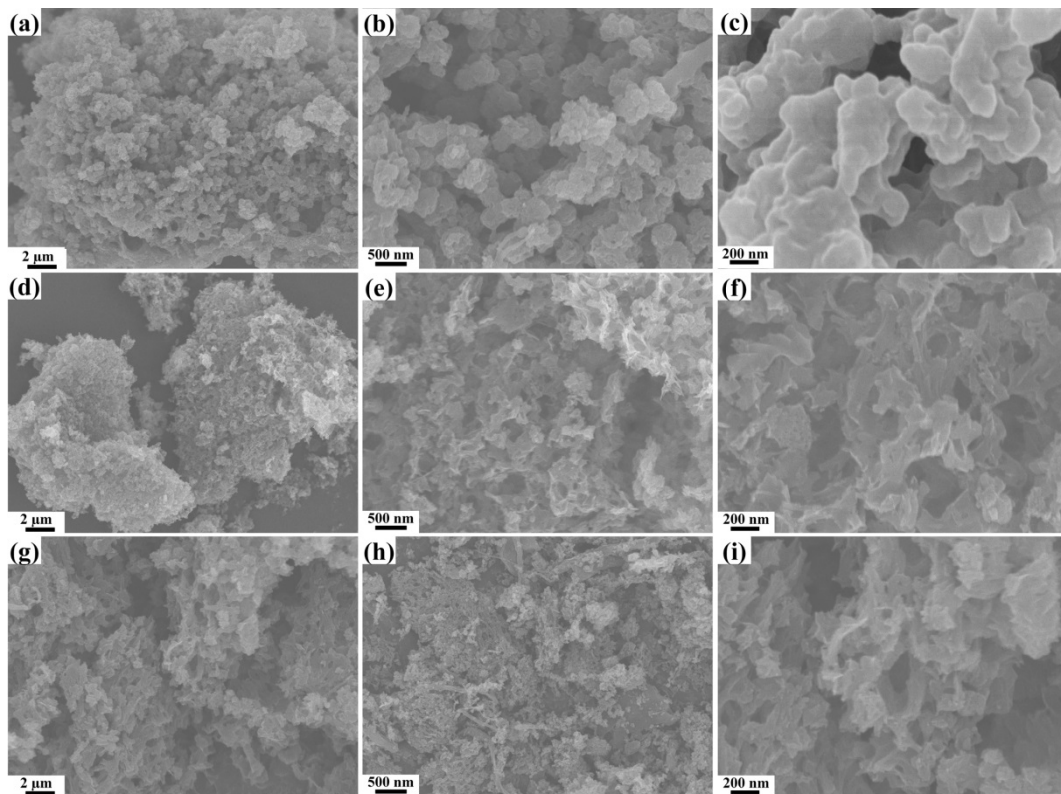


Fig. S5. SEM images of (a-c) Fe/N@CNF-700, (d-f) Fe/N@CNF-800, (g-i) Fe/N@CNF-900 at low and high magnifications, respectively.

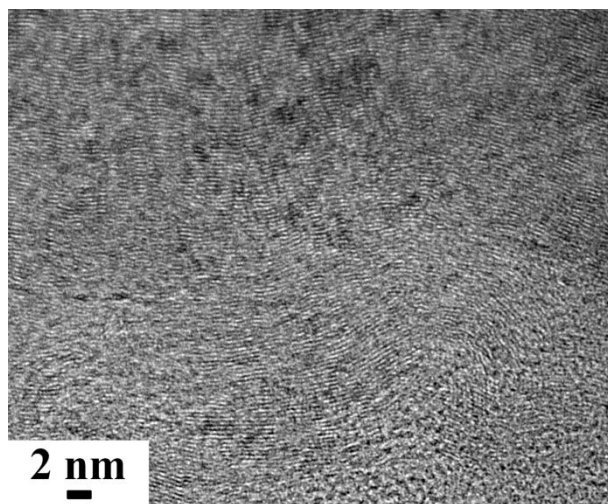


Fig. S6. HRTEM image of Fe/N@CNF-800.

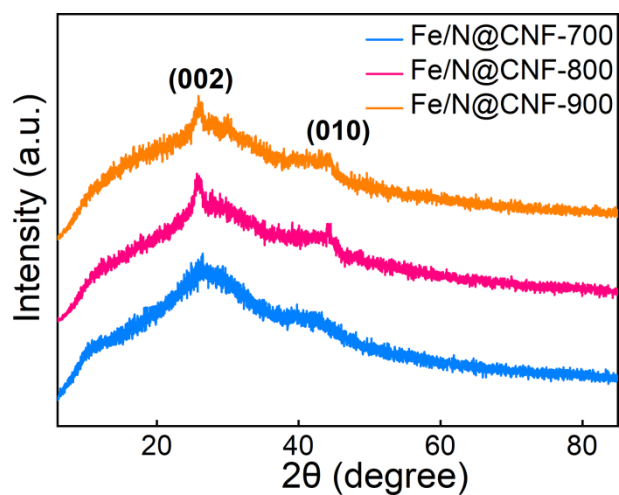


Fig. S7. XRD patterns of the Fe/N@CNFs.

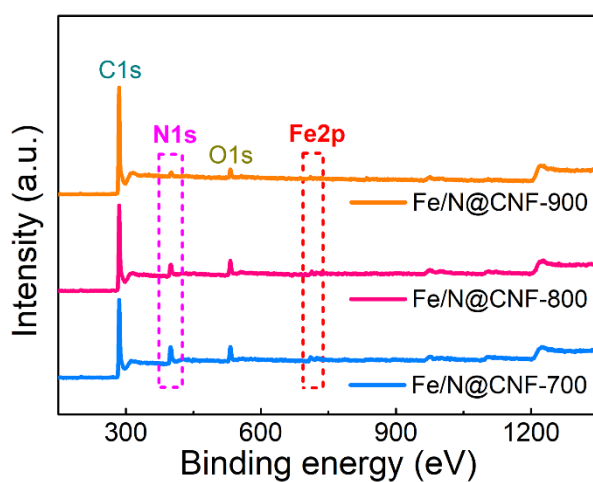


Fig. S8. XPS survey of Fe/N@CNF-700, Fe/N@CNF-800 and Fe/N@CNF-900 catalysts.

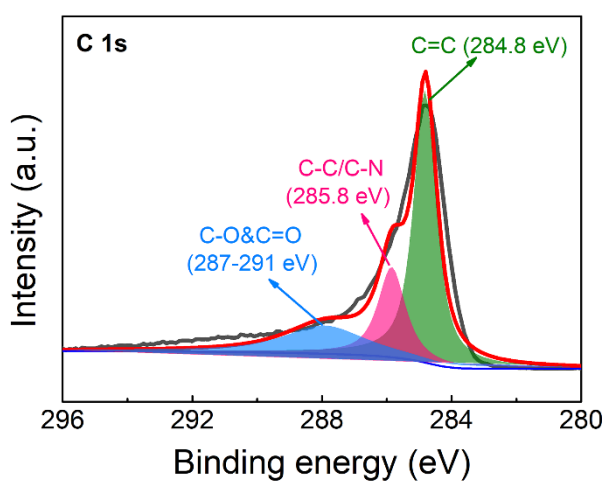


Fig. S9. High-resolution C 1s XPS spectra of Fe/N@CNF-800.

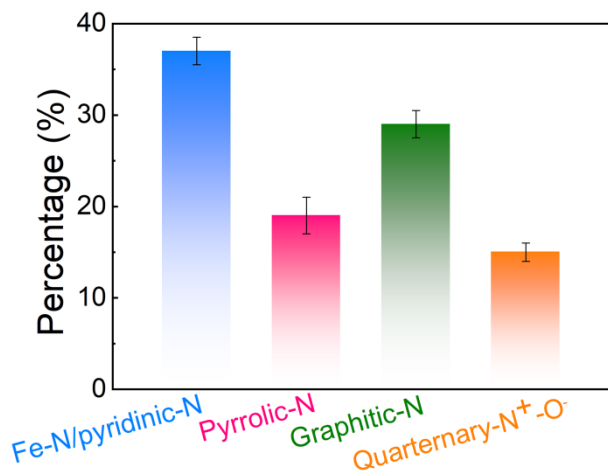


Fig. S10. The proportion of different doped-N types of Fe/N@CNF-800 catalyst.

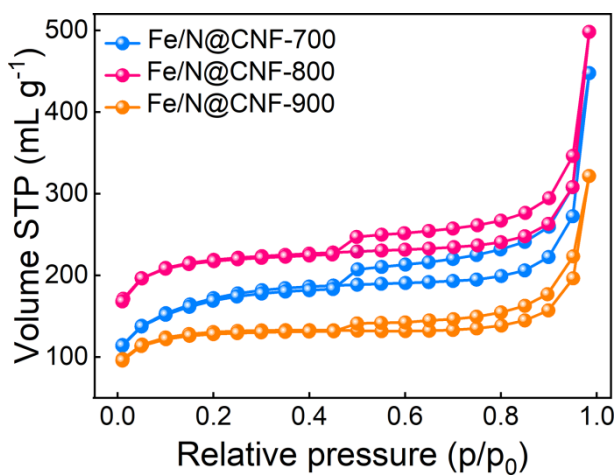


Fig. S11. Nitrogen adsorption/desorption isotherm of Fe/N@CNFs.

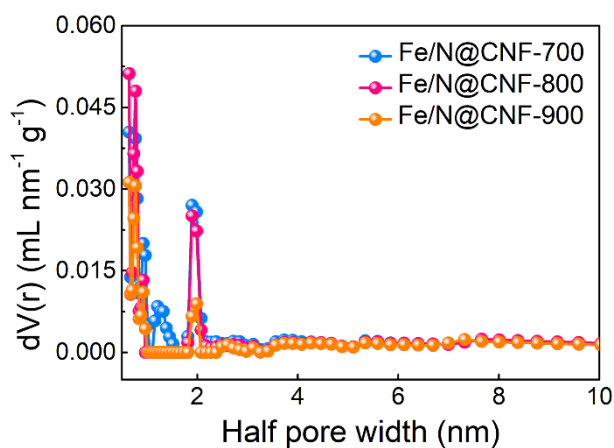


Fig. S12. The pore size distribution of the Fe/N@CNFs.

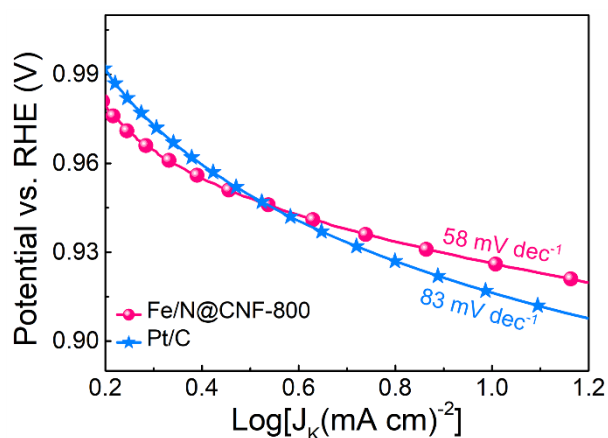


Fig. S13. Tafel curves of the different samples from corresponding ORR LSV curves.

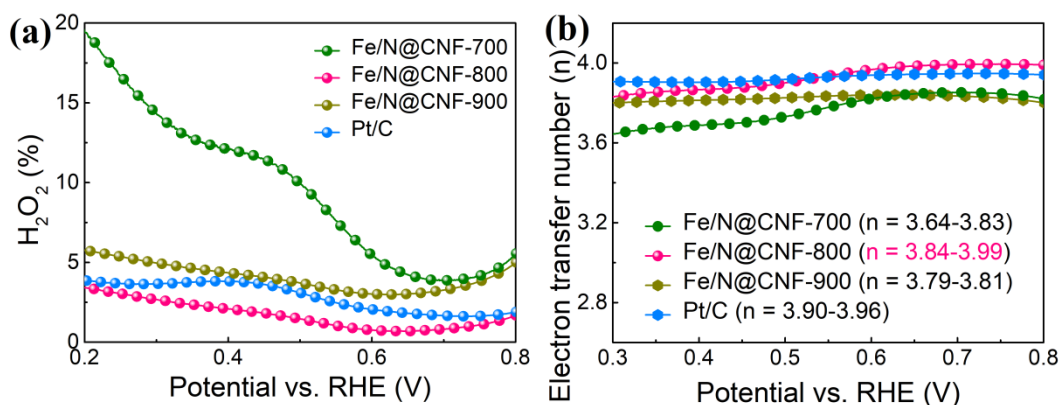


Fig. S14. (a) H_2O_2 yields and (b) calculated electron-transfer numbers of the FeN@CNF-800 derived from RRDE polarization curves in 0.1 M O_2 -saturated KOH solution, 1600 rpm.

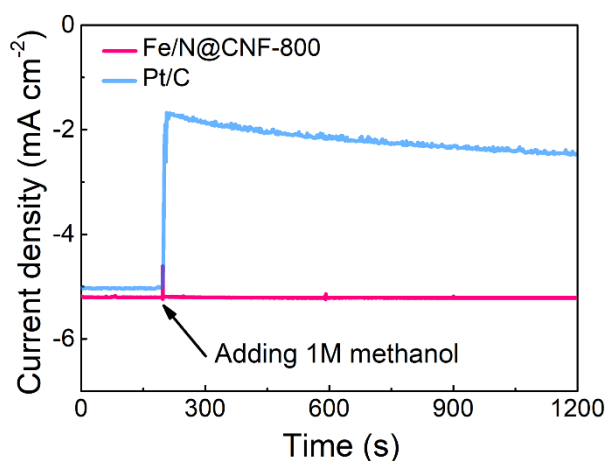


Fig. S15. (a) Chronoamperometric responses of Fe/N@CNF-800 and Pt/C catalysts upon addition of 1 M methanol, respectively.

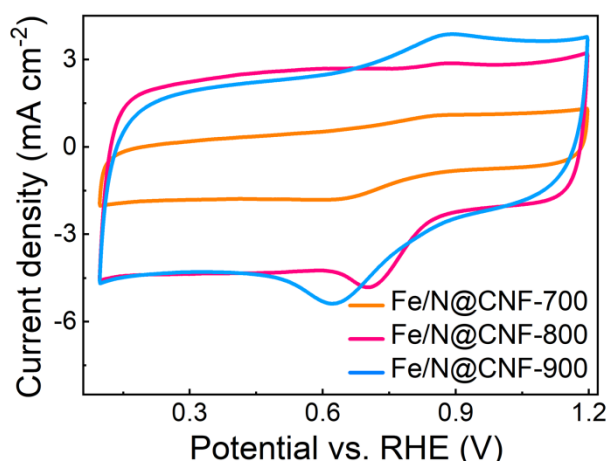


Fig. S16. CV curves of the Fe/N@CNFs in 0.1 M H₂SO₄ at scan rate 50 mV s⁻¹.

Table S1. Elemental compositions of Fe/N@CNFs determined by XPS results.

samples	C [at%]	N [at%]	Fe [at%]
Fe/N@CNF-700	77.24	14.54	1.21
Fe/N@CNF-800	85.17	4.84	0.99
Fe/N@CNF-900	91.03	4.11	0.51

Table S2. Comparison of our Fe/N@CNF-800 catalyst with some reported Fe-based ORR catalysts in 0.1 M KOH electrolyte.

catalysts	E _{onset} (V vs.RHE)	E _{1/2} (V vs.RHE)	J _L (mA cm ⁻²)	Ref.
Fe ₃ C-FeN/NC-2	0.95	0.82	5.02	[1]
Fe ₃ C/Fe ₂ O ₃ @N-CNTs	0.97	0.88	6.01	[2]
Fe-Zn-SA/NC	0.93	0.85	4.83	[3]
FeCo-NPs/NC	0.91	0.82	5.15	[4]
Fe-N/C-800	1.00	0.84	5.19	[5]
Ag-CoFe@NC-700	0.96	0.83	5.31	[6]
Fe-SASC	1.00	0.87	5.62	[7]
Co ₃ Fe ₇ /N, Mn-PC	0.98	0.87	5.87	[8]
Fe-NC/rOCNT	0.98	0.87	5.76	[9]
Timb-Fe ₅ -C	0.99	0.89	5.36	[10]
Fe _{Fe} -O-Fe-UP/CA	1.08	0.93	5.71	[11]

FeNC-NW	1.02	0.92	6.01	[12]
meso-Fe-N-C	0.92	0.85	5.68	[13]
Ni ₃ Fe-GA ₁	0.93	0.80	4.52	[14]
Fe ₂₀ @N/HCSs	0.95	0.85	5.75	[15]
Co ₃ Fe ₇ @Fe ₂ N/rGO	0.95	0.79	5.41	[16]
MPC@PhFe	0.99	0.86	5.33	[17]
Fe/N@CNF-800	1.02	0.89	5.15	this work

Table S3. Comparison of some recently reported Fe-based ORR catalysts in acid condition.

Catalyst	ORR E _{onset} (V vs.RHE)	ORR E _{1/2} (V vs.RHE)	J _L (mA cm ⁻²)	Electrolyte	Ref.
Fe-Zn-SA/NC	0.87	0.78	4.72	0.1 M HClO ₄	[3]
HSAC/Fe-3	0.94	0.81	4.53	0.5 M H ₂ SO ₄	[18]
FeNC-NW	0.90	0.82	5.51	0.1 M HClO ₄	[12]
HP-FeN ₄	0.95	0.80	5.78	0.1 M HClO ₄	[19]
FeN ₄ /HOPC-c-1000	0.90	0.78	4.52	0.5 M H ₂ SO ₄	[20]
Fe-N-C/FeN	0.89	0.78	8.81	0.1 M HClO ₄	[21]
FeNC-BP	0.84	0.69	5.54	0.1 M H ₂ SO ₄	[22]
Co-Fe-S@NSRPC	0.86	0.80	5.01	0.5 M H ₂ SO ₄	[23]
NGM-800	0.86	0.78	4.24	0.1 M HClO ₄	[24]
Fe/N@CNF-800	0.92	0.78	4.48	0.5 M H₂SO₄	This work

Table S4. Comparison of the performance of Zn-air batteries with our Fe/N@CNF-800 catalyst and Fe-based catalysts.

air catalysts	open-circuit voltage [V]	power density [mW cm ⁻²]	Ref.
SA-Fe/NC	-	91	[25]
Si-Fe/S/N-RH ₃	1.53	86	[26]
A-Fe-NC	1.45	132	[27]
Fe _{0.5} Ni _{0.5} @N	1.48	85	[28]
CoFe-Co@PNC	1.46	153	[29]
Co _{0.7} Fe _{0.3} @NC	1.45	86	[30]
Fe-N-C/N-OMC	1.55	113	[31]
CoFeP@C	-	144	[32]
FeS/Fe ₃ C@NS	1.46	91	[33]
SA-Fe-N _x -MPC	1.53	130	[34]
Ni ₃ FeN	1.55	-	[35]
Co/CoO@FeNC	1.42	133	[36]

Fe/Co-N _x -C	1.42	152	[37]
FeNSC800	1.52	60	[38]
HCSC-IV-H	1.43	105	[39]
FeCo-NPC	1.49	93	[40]
Fe/N@CNF-800	1.51	164	This work

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