# **Electronic Supplementary Material**

# Precursor-driven structural tailoring of iron oxychloride for enhanced heterogeneous Fenton activity

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### 1. SEM characterization



Fig. S1.The SEM images of the hematite precursors with different milling durations (a-d) and their derived FeOCl (e-l)

Since FeOCl adopts an orthorhombic structure, the formula for the angle of each

crystal plane follows the formula eq. S1-eq. S2.

$$\cos \varphi = \frac{\frac{h_1 h_2}{a^2} + \frac{k_1 k_2}{b^2} + \frac{l_1 l_2}{c^2}}{\sqrt{\left(\frac{h_1^2}{a} + \frac{k_1^2}{b} + \frac{l_1^2}{c}\right)\left(\frac{h_2^2}{a} + \frac{k_2^2}{b} + \frac{l_2^2}{c}\right)}}$$
eq. S1

$$\cos \varphi = \frac{\frac{\pm 1}{b^2}}{\sqrt{(\frac{1^2}{a} + \frac{1^2}{b})(\frac{1^2}{b})}}$$
 eq. S2

a, b, c are the unit cell parameters of FeOCl ;a=3.7802 Å; b=7.917 Å;c=3.302 Å.[1]

It can be calculated that the angle between the (110/1-10) crystal plane and the

(010) crystal plane is 115°, which appears on the side of the (010) crystal plane. As seen in Fig. S1(i-l), the side of pristine FeOCl is smooth and contains no edges. Combined with the TEM results, the basal plane surface exposed on pristine FeOCl is (010), and its side should be (200) crystal plane. After the precursors ground for 30 minutes, the side planes appeared. The angle between the inclined face and the (010) surface is 116.6°, which is close to the theoretical value of 115°. Therefore, it was proposed that the inclined plane was attributed to the (110/1-10) crystal plane. As the particle size decreased, it could be observed that a similar phenomenon of the edge and oblique planes appeared on the side of FeOCl, which could be judged as high energy (110/1-10) crystal plane.

#### 2. Infrared vibration of Fe-O



**Fig. S2.** Fitted vibration peaks of infrared Fe-O bonds with hematite precursors under grinding for different durations.

FTIR wavenumber	440 cm <sup>-1</sup>	480 cm <sup>-1</sup>	540 cm <sup>-1</sup>	630 cm <sup>-1</sup>
Initial Fe <sub>2</sub> O <sub>3</sub>	0.089	0.242	0.631	0.132
Fe <sub>2</sub> O <sub>3</sub> - Grind 30min	0.042	0.220	0.566	0.190
Fe <sub>2</sub> O <sub>3</sub> -Grind 120min	0.020	0.211	0.526	0.231
Fe <sub>2</sub> O <sub>3</sub> -Grind 12h	0.015	0.201	0.403	0.305

 Table S1. The percentage of each IR peak area at different wavenumbers for hematite grinded under different grinding durations.

# 3. particle size and specific surface area of different FeOCl

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Materials	LPSA(MV,µm)	SEM(µm)	BET(m <sup>2</sup> /g)
FeOC1-P	10.48	3-15	8.93
FeOCl-30nm	6.47	3-9	/
FeOCl-0.5h	9.85	2-10	/
FeOCl-2h	7.8	2-7.8	/
FeOCl-12h	4.36	3	34.28

 Table S2. Characterization of particle size and specific surface area of different FeOCl.



Fig. S3. The nitrogen isotherm adsorption-desorption curves of pristine FeOCl and FeOCl-12h.

#### 4. The intensity diffraction peak ratio from XRD patterns



**Fig. S4.** (a) The XRD patterns of FeOCl synthesized from hematite subjected to different milling times. (b) The diffraction peaks of different FeOCl at high Bragg angles.

Intensity ratios	from XRI	) Initial Fe <sub>2</sub>	O3 Fe2O3-3	0min	Fe <sub>2</sub> O <sub>3</sub> - 120min	Fe <sub>2</sub> O <sub>3</sub> -12h
L (104)-L (110)	Area	1.39	1.35		1.28	1.32
1 (104):1 (110)	Height	1.62	1.45		1.36	1.19
Intensity ratio XRD	os from	FeOCl-P	FeOCl- 30nm	FeOCl- 30min	FeOCl- 120min	FeOCl- 12h
L (010) L (110)	Area	500	66.67	21.74	11.63	6.29
1 (010):1 (110)	Height	500	37.04	25.64	12.82	7.30

Table S3. Diffraction peak intensity ratio of hematite and FeOCl from corrected XRD

Based on the corrected XRD pattern, the (110) and (010) intensity ratios for different FeOCl were calculated. The proportion of  $I_{(110)}$  increases with the reduced sizes of FeOCl particles, which indicates that the growth orientation of small-sized FeOCl in the [110] direction was increasing. Combined with the SEM images in Fig. S1, the (110) crystal plane was gradually exposed to the surface as the FeOCl particle size became smaller.

# 5. The adsorption capacity of the obtained FeOCl series materials



**Fig. S5.** Activity of different FeOCl for adsorption of phenol. Reaction conditions: Phenol concentration of 50 ppm; catalyst dosage of 500 ppm; pH=4.0 (4mM HAc-NaAc); 25°C.

# 6. EPR signal



Fig. S6. EPR signals obtained in methanol containing 180 mM DMPO + 500 mg/L FeOCl + 30mM H<sub>2</sub>O<sub>2</sub>.

# 7. Surface energy calculation

facet	E <sub>bulk</sub> (eV)	$E_{slab}^{unrelax}(eV)$	$E_{slab}^{relax}(eV)$	$A(Å^2)$	n	$\gamma$ (J/m <sup>2</sup> )
100		-152.206	-152.68	26.163	5	0.0315522
110	-30.961	-152.191	-152.543	28.569	5	0.0334278
010		-154.74	-154.77	12.11		0.00012

Table S4. Surface energy calculation of (100), (110), (010) crystal planes



**Fig. S7.** Surface structures of crystal plane (a) (010) and (b) (110) of FeOCl Surface structure for evaluating adsorption energy. The dotted lines indicate the lattice surfaces.

## 8. The detailed XPS data of tailored FeOCl with different sizes.



Fig. S8. XPS spectrum of Fe2p<sub>3/2</sub> from pristine FeOCl-P and FeOCl-12 h.



Fig. S9. XPS spectrum of (a) O1s and (b) Cl 2p from pristine FeOCl-P and FeOCl-12 h.

	-	Atomic percentage of XPS (%)				
Different FeOC	l Fe		Cl	0		
FeOCl-Pristine	6.2	5	8.09	10.88		
FeOCl-0.5h	6.4	4	5.34	13.45		
FeOCl-2h	6.5	0	5.19	13.57		
FeOCl-12h	6.5	6	4.63	14.05		
Catalysts		<b>B.E.</b> (eV)	Area	Percentage		
	Fe(III)-O	711.0	22193.3	37.3%		
FeOCl-Pristine	Fe(III)-Cl	712.3	37312.1	67.2%		
	Fe(II)	708.52	1283	1.3%		
FeOCl-0.5h	Fe(III)-O	710.9	29086.9	43.9%		
	Fe(III)-Cl	712.3	36277.5	54.8%		
	Fe(II)	708.6	1316	2.03%		
FeOCl-2h	Fe(III)-O	710.8	30312.3	46.8%		
	Fe(III)-Cl	712.3	33087.8	51.17%		
FeOCl-12h	Fe(II)	708.6	1328	2.05%		
	Fe(III)-O	710.8	33025	50.98%		
	Fe(III)-Cl	712.2	30416	46.97%		

**Table S5**. Surface element content calculated by XPS and the peak-fitting result of Fe  $2p_{3/2}$  spectraof each size FeOCl

#### 9. Intermediate/product variation versus time and phenol degradation path



Fig. S10. Intermediate products detected in the phenol degradation process in this Fenton-like system. 50 ppm phenol + 500 ppm FeOCl-12h + 5.9 mg/L NaCl + 30 mM H<sub>2</sub>O<sub>2</sub> (pH = 4, 4 mM HAc-NaAc buffer, 25 °C).



**Fig. S11.** Total organic carbon (TOC) variation in the phenol degradation process in this Fenton-like system. 50 ppm phenol + 500 ppm FeOCl-12h + 5.9 mg/L NaCl + 30 mM H<sub>2</sub>O<sub>2</sub> (pH = 4, 4 mM HAc-NaAc buffer, 25 °C).



Fig. S12. The proposed reaction path of phenol degradation in this Fenton-like system.

#### 10. Stability of FeOCl structure and properties

The cycling experiments and structural characterizations evaluated the stability of the fabricated FeOCl. After each round of experiments, the catalyst was separated by filtration using a 0.22  $\mu$ m filter, washed with deionized water and acetone repeatedly three times, and placed in a vacuum oven at 40 °C for the next round of the experiment.



Fig. S13. Cycling experiment of the fabricated FeOCl. Reaction condition: 50 ppm phenol + 500 ppm FeOCl + 30 mM  $H_2O_2$  (pH = 4, 4 mM HAc-NaAc buffer, 25 °C).



**Fig. S14.** (a)XRD pattern of FeOCI-12h before and after reaction; SEM images of FeOCI (b) before (c) the after the reaction; (d) TEM and (e) SAED of the reacted FeOCI.

Identical XRD peaks were observed after the reaction, consistent with the standard PDF card JCPDS No.39-0612 of FeOCI. Consistent results of SEM, TEM, and SAED characterization were also obtained, indicating the high robustness of the FeOCI catalyst during the reaction.

#### **11. Different pH effects**



Fig. S15. (a) DMPO/OH · of FeOCl-12h in different pH solutions. (b) The decomposition of H<sub>2</sub>O<sub>2</sub> in different pH solutions. (c, d) pCBA probe experiment of FeOCl-12h in different pH solutions. 180 mM DMPO; 30mM H<sub>2</sub>O<sub>2</sub>; 500 ppm FeOCl materials; 0.06 mM pCBA.

The results revealed that the fabricated FeOCl exhibited a higher capability of activating  $H_2O_2$  and generating hydroxyl radicals under lower pHs with lower capability at higher pHs. Nevertheless, even under pH = 7, the regulated FeOCl could activate  $H_2O_2$  to generate OH·, which was often not observed on Fe-based materials.

# 12. Comparison with other catalyst parameters

catalyst	рН	Initial conc (mg L <sup>-</sup> <sup>1</sup> )	Conc. of catalyst and H <sub>2</sub> O <sub>2</sub>	Removal of phenol and time	Leaching of Fe (mg L <sup>-1</sup> ) (ratio of Fe atoms%)	Ref.
	4	50	0.1g/L, 6mM	90%, 16min	2(2%)	
Dendritic Fe <sup>0</sup>	3.5	50	0.1g/L, 6mM	90%, 3min	8(8%)	[2]
Fe <sub>3</sub> O <sub>4</sub> /MWCNTs	3	100	1g/L, 10mM	100%, 120min	2.5(1.38%)	[3]
FeOCl	4	100	0.2g/L, 15.6mM	100%, 30min	0.57- 1.25(0.54- 1.2%)	[4]
Fe <sub>2</sub> O <sub>3</sub> -ZrO <sub>2</sub>	6	100	0.8g/L, 112mM(60°C)	100%, 210min	<0.5%	[5]
	3	100	1g/L, 14.7mM	100%, 30min	5.0-27(0 .92-4.95%)	[6]
Schwertmannte	5	100	1g/L, 14.7mM	100%, 6h	2.5-13(0.46- 2.47%)	- [0]
	3	50	1g/L, 7mM	100%, 7h	1.7(0.26%)	
Fe-clay	4	50	0.5g/L, 10mM	100%, 10min	2.54(0.28%)	[7]
Fe-Pd@C	5	50	0.5g/L, 10mM	99%, 60min	0.51(0.06%)	101
	6	50	0.5g/L, 10mM	95%, 60min	0.48(0.05%)	- [ð]
FeOCl-12h	4	50	0.5g/L, 30mM	99%, 60min	0.47(0.04%)	this work

Table S6. Comparison study of phenol degradation in Fenton reaction using different catalysts

### 13. The effect of leached Fe and Cl

After	reaction	FeOCl-P	FeOCl- 30nm	FeOCl-0.5h	FeOCl-2h	FeOCl-12h
Fe leaching	Concentration (mg/L)	0.29	0.37	0.40	0.44	0.47
F	Proportion (%)	0.11	0.14	0.15	0.17	0.18
Cl leaching	Concentration (mg/L)	4.10	4.70	5.10	5.00	5.90
	Proportion (%)	2.48	2.85	3.09	3.03	3.57

Table S7. The concentration of leaching Fe and Cl in the reaction solution.

We selected the largest leached iron concentration (0.47 mg/L) to analyze the effect of leached iron on H<sub>2</sub>O<sub>2</sub> activation. The formation of hydroxyl radicals (OH·) was measured using p-chlorobenzoic acid (pCBA) as a probe.



**Fig. S16.** Effect of leached iron on a system of  $H_2O_2$  activation. Reaction condition: 0.06 mM pCBA + 500 ppm FeOCl + 0.47 mg/L Fe<sup>2+</sup> + 30 mM H<sub>2</sub>O<sub>2</sub> (pH = 4, 4 mM HAc-NaAc buffer, 25



**Fig. S17.** Effect of leached Cl<sup>-</sup> in the  $H_2O_2$  activation system. Reaction condition: 50 ppm phenol + 500 ppm FeOCl + 5.9 mg/L NaCl + 30 mM  $H_2O_2$  (pH = 4, 4 mM HAc-NaAc buffer, 25 °C).

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