

# Electronic Supplementary Material

## Asymmetric copolyimide membranes fabricated by nonsolvent-induced phase separation for He/CH<sub>4</sub> and He/N<sub>2</sub> separation

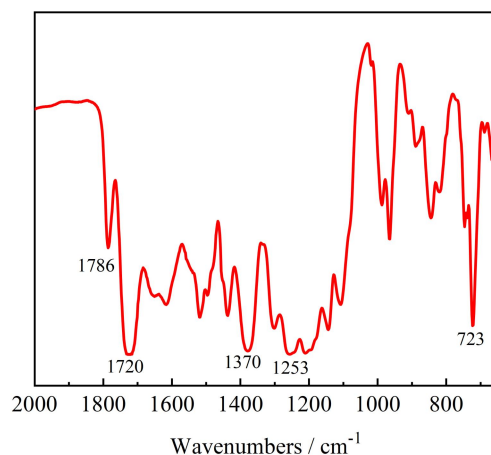
Ying Li<sup>1,2\*</sup>, Lu Wang<sup>1\*</sup>, Junyan Xie<sup>1</sup>, Yong Dai<sup>1</sup>, Xuehong Gu<sup>1</sup>, Xuerui Wang (✉)<sup>1</sup>

<sup>1</sup> State Key Laboratory of Materials-Oriented Chemical Engineering, College of Chemical Engineering, Nanjing Tech University, Nanjing 211816, China

<sup>2</sup> Quzhou Membrane Material Innovation Institute, Quzhou 324000, China

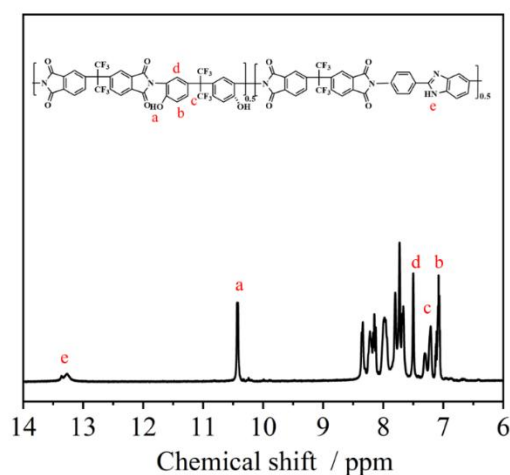
E-mail: x.wang@njtech.edu.cn

\* These authors contributed equally to this work.



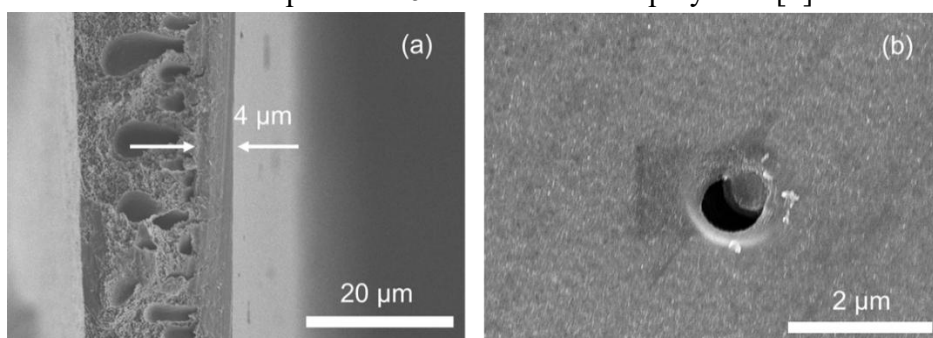
**Fig. S1** ATR-FTIR spectra of 6FDA-APAF<sub>0.5</sub>-BIA<sub>0.5</sub> copolyimide membrane.

The chemical structures of 6FDA-APAF<sub>0.5</sub>-BIA<sub>0.5</sub> copolyimide were confirmed by ATR-FTIR (Fig. S1). Characteristic imide absorption bands were observed at around 1786 cm<sup>-1</sup> (imide carbonyl asymmetric stretching), 1718 cm<sup>-1</sup> (imide carbonyl symmetric stretching) [1] and 1253 cm<sup>-1</sup> (CF<sub>3</sub> stretching) [2]. The bands at 1370 cm<sup>-1</sup> and 723 cm<sup>-1</sup> were transverse stretching and out-of-plane bending of C-N-C groups, respectively [3].

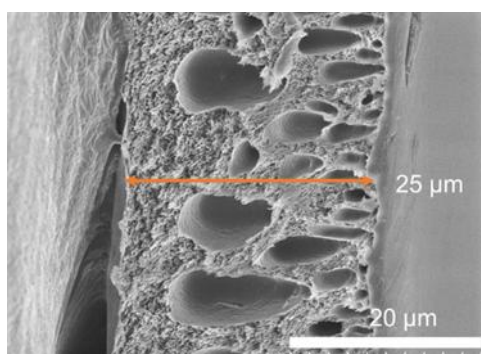


**Fig. S2**  $^1\text{H}$  NMR spectroscopy of 6FDA-APAF<sub>0.5</sub>-BIA<sub>0.5</sub> copolyimide.

The presence of APAF was well demonstrated by the chemical shifts at 10.5 ppm, 7.1 ppm, 7.2 ppm, and 7.5 ppm (a, b, c, and d). The copolyimide exhibited an additional signal at 13.3 ppm (e) due to  $-\text{N}-\text{H}$  in the benzimidazole rings. The results were in accord with  $^1\text{H}$  NMR spectra of 6FDA-APAF-BIA polymers [1].



**Fig. S3** Cross-sectional SEM images of (a) 30 wt.%. Top view of (b) 30 wt.%.



**Fig. S4** Cross-sectional SEM image of the whole membrane.

**Table S1** Molecular weight data.

No.	$M_n / 10^4 \text{ g mol}^{-1}$	$M_w / 10^4 \text{ g mol}^{-1}$	PDI / $M_w/M_n$
6FDA-APAF-BIA	1.38	2.95	2.14

**Table S2** Dense membrane properties.

Density / $\text{g}\cdot\text{cm}^{-3}$	FFV / -	Thickness / $\mu\text{m}$	$P_{\text{He}}$ / <i>Barrer</i>	$\alpha_{\text{He/CH}_4}$ / -	$P_{\text{He}}$ / <i>Barrer</i>	$\alpha_{\text{He/N}_2}$ /
1.584	0.149	60	72	101	74	72

**Table S3** Physical properties of polymer, solvents and non-solvents.

	Molar volume $\text{mL/mol}$	$\rho$ / $\text{g/mL}$	$\delta$ / $\text{MPa}^{1/2}$	$\chi$ parameter with polymer	Miscibility	$\chi$ parameter with water
Polymer	N.A.	1.290	21.3	N.A.	N.A.	5.10
NMP	96.60	1.032	22.7	0.08	Yes	0.51
THF	81.90	0.889	19.5	0.11	Yes	1.39
Ethanol	58.39	0.789	26.5	0.63	No	1.05
Water	18.01	1.000	47.8	5.10	No	N.A.

**Table S4** Linear fitting parameters of and activation energy for He/N<sub>2</sub> and He/CH<sub>4</sub> mixture permeation and single gas permeation in M7 membrane at 0.1 MPa.

		Linear fitting parameters		$E_{\text{act}}$
		Intercept (a)	Slope ( $-\frac{E_{\text{act},i}}{R}$ )	$\text{kJ mol}^{-1}$
He/N <sub>2</sub>	He	-7.74	-1.00	8.3
	N <sub>2</sub>	-6.15	-1.72	14.3
He/CH <sub>4</sub>	He	-7.61	-0.97	8.1
	CH <sub>4</sub>	-6.03	-1.83	15.2
	He	-7.91	-0.98	8.1
Single gas	N <sub>2</sub>	-6.73	-1.84	15.3
	CH <sub>4</sub>	-7.16	-2.10	17.5

**Table S5** Comparison of the performance of the 6FDA-APAF<sub>0.5</sub>-BIA<sub>0.5</sub> membranes with state-of-the-art membranes.

Membranes	He/CH <sub>4</sub> system			He/N <sub>2</sub> system			Ref
	$P_{\text{He}} /$ GPU	$S_{\text{He/CH}_4}$ /-	$\alpha_{\text{He/CH}_4}$ /-	$P_{\text{He}} /$ GPU	$S_{\text{He/N}_2}$ /-	$\alpha_{\text{He/N}_2}$ /-	
TR-6FDA-APAF	2.4	37.2	N.A.	2.4	26.4	N.A.	[4]
6FDA-APAF-BIA	1.8	317.4	N.A.	1.8	121.7	N.A.	[1]
Nafion-117	32.0	56.3	N.A.	32.0	94	N.A.	[5]
Poly(PFMD)	7.0	1650.0	N.A.	7.0	295.8	N.A.	[6]
Poly(PFMMD)	11.2	280.0	N.A.	11.2	72.7	N.A.	
PIM-EA-TB	14.2	3.7	N.A.	14.2	4.90	N.A.	[7]
PIM-SBI-TB	5.6	2.0	N.A.	5.6	3.8	N.A.	
Fluorinated PIM	202	61.2	N.A.	202	36.1	N.A.	[8]
FPIM-5	16.6	3770	N.A.	16.6	857	N.A.	[9]
Cellulose acetate	28.0	40.0	N.A.	28.0	46.7	N.A.	[10]
Polysulphone	0.52	49.0	N.A.	0.52	52.0	N.A.	[11]
PBDI	46	1000	N.A.	46	295	N.A.	[12]
STT	37.1	87.0	63.5	35.4	20.0	11.7	[13]
SAPO-34	554.1	N.A.	13.8	N.A.	N.A.	N.A.	[14]
DD3R	13.6	79.0	59.0	13.6	2.9	N.A.	[15]
TR-6FDA-APAF-Cardo	14.1	64	66.4	13.7	52	54.4	[16]
TR-6FDA-APAF <sub>0.5</sub> -Cardo 0.5/Al <sub>2</sub> O <sub>3</sub>	40.0	71.2	74.3	40.0	60.0	50.0	
Membrane M7	85	124	80	86	74	60	This work
Membrane M11	88	N.A.	75	89	N.A.	54	
Membrane M12	80	N.A.	80	83	N.A.	59	
Membrane M13	91	N.A.	74	92	N.A.	52	
Membrane M14	76	N.A.	83	79	N.A.	61	

## References

- Zhuang Y, Seong J, Lee W H, Do Y, Lee M J, Wang G, Guiver M, Lee Y M. Mechanically tough, thermally rearranged (TR) random/block poly(benzoxazole-co-imide) gas separation membranes. *Macromolecules*, 2015, 48: 5286-5299
- Mariola C, Doherty C M, Hill A J, Moo L Y. Cross-linked thermally rearranged poly(benzoxazole-co-imide) membranes for gas separation. *Macromolecules*, 2013, 46: 8179-8189
- Gándara B C, Calle M, Jo H J, Hernández A, Campa J G d l, Abajo J d, Lozano A E, Lee Y M. Thermally rearranged polybenzoxazoles membranes with biphenyl

- moieties: Monomer isomeric effect. *Journal of Membrane Science*, 2014, 450: 369-379
4. Calle M, Lee Y M. Thermally Rearranged (TR) Poly(ether–benzoxazole) Membranes for Gas Separation. *Macromolecules*, 2011, 44: 1156-1165
  5. Choi S H, Qahtani M S, Qasem E A. Multilayer thin-film composite membranes for helium enrichment. *Journal of Membrane Science*, 2018, 553: 180-188
  6. Yavari M, Fang M, Nguyen H, Merkel T C, Lin H, Okamoto Y. Dioxolane-based perfluoropolymers with superior membrane gas separation properties. *Macromolecules*, 2018, 51: 2489-2497
  7. Carta M, Evans R M, Croad M, Rogan Y, Jansen J C, Bernardo P, Bazzarelli F, McKeown N B. An efficient polymer molecular sieve for membrane gas separations. *Science*, 2013, 339: 303-307
  8. Seong J G, Hee W L, Lee J, Lee S Y, Do Y S, Bae J Y, Moon S J, Park C H, Jo H J, Kim J S, Lee K R, Hung W S, Lai J Y, Ren Y, Roos C J, Lively R P, Lee Y M. Microporous polymers with cascaded cavities for controlled transport of small gas molecules. *Science Advances*, 2021, 7: eabi9062
  9. Ma X, Li K, Zhu Z, Dong H, Lv J, Wang Y, Pinnau I, Li J, Chen B, Han Y. High-performance polymer molecular sieve membranes prepared by direct fluorination for efficient helium enrichment. *Journal Of Materials Chemistry A*, 2021, 9: 18313-18322
  10. Gantzel P K, Merten U. Gas separations with high-flux cellulose acetate membranes. *Industrial & Engineering Chemistry Process Design and Development*, 1970, 9: 331-332
  11. McHattie J S, Koros W J, Paul D R. Gas transport properties of polysulphones: 2. Effect of bisphenol connector groups. *Polymer*, 1991, 32: 2618-2625
  12. Wang X, Shan M, Liu X, Wang M, Doherty C M, Osadchii D, Kapteijn F. High-performance polybenzimidazole membranes for helium extraction from natural gas. *ACS Applied Materials & Interfaces*, 2019, 11: 20098-20103
  13. Gong C, Peng X, Zhu M, Zhou T, You L, Ren S, Wang X, Gu X. Synthesis and performance of STT zeolite membranes for He/N<sub>2</sub> and He/CH<sub>4</sub> separation. *Separation and Purification Technology*, 2022, 301: 121927
  14. Denning S, Lucero J, Koh C A, Carreon M A. Chabazite zeolite SAPO-34 membranes for He/CH<sub>4</sub> separation. *ACS Materials Letters*, 2019, 1: 655-659
  15. Zhang P, Gong C, Zhou T, Du P, Song J, Shi M, Wang X, Gu X. Helium extraction from natural gas using DD3R zeolite membranes. *Chinese Journal of Chemical Engineering*, 2021, 49: 122-129
  16. Wang L, Li Y, Zhang P, Chen X, Nian P, Wei Y, Lu H, Gu X, Wang X. Thermally rearranged poly(benzoxazole-co-imide) composite membranes on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> support

for helium extraction from natural gas. *Journal of Membrane Science*, 2022, 657: 120614